

Safety and Environmental Issues for FPSO Projects

Dave Ashton - Atkins

dave.ashton@atkinsglobal.com

Agenda

- ❑ Formal safety assessment in design - why? how?
- ❑ Getting safety into the early design – inherently safe design
- ❑ FPSO major hazards
 - Hazard Management (Prevention, Control / Mitigate, Recovery)
 - Common concerns from Formal Safety Assessments (FSA)
- ❑ Environmental concerns and related issues

Formal Safety Assessment – Why?

- ❑ Major Accident Events will continue to occur.



Ship Collision Followed by Major Fire



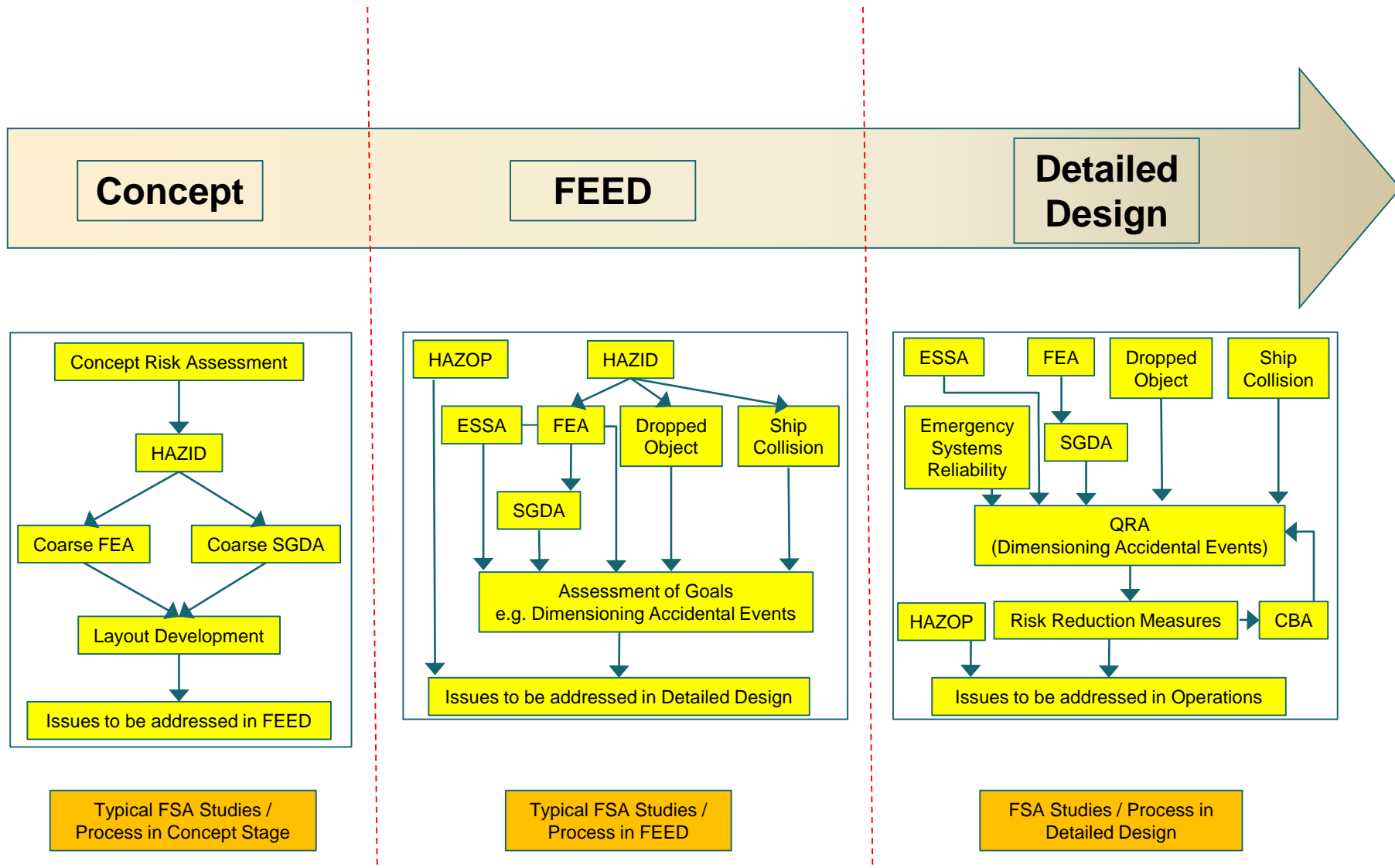
Cargo Tank Explosion



Riser Fire Engulfing Platform

- Safety evaluations carried out to confirm design achieves safety goals
- Primary aim is to pinpoint targets for risk reduction measures which can be assessed and included where reasonably practicable
- In this way safety analyses during design can reduce the **frequency** of accidents occurring and reduce the **consequences** of an accident
- FSA also contributes to ensuring safe and secure physical environment and in minimising pollution

Formal Safety Assessment – How?



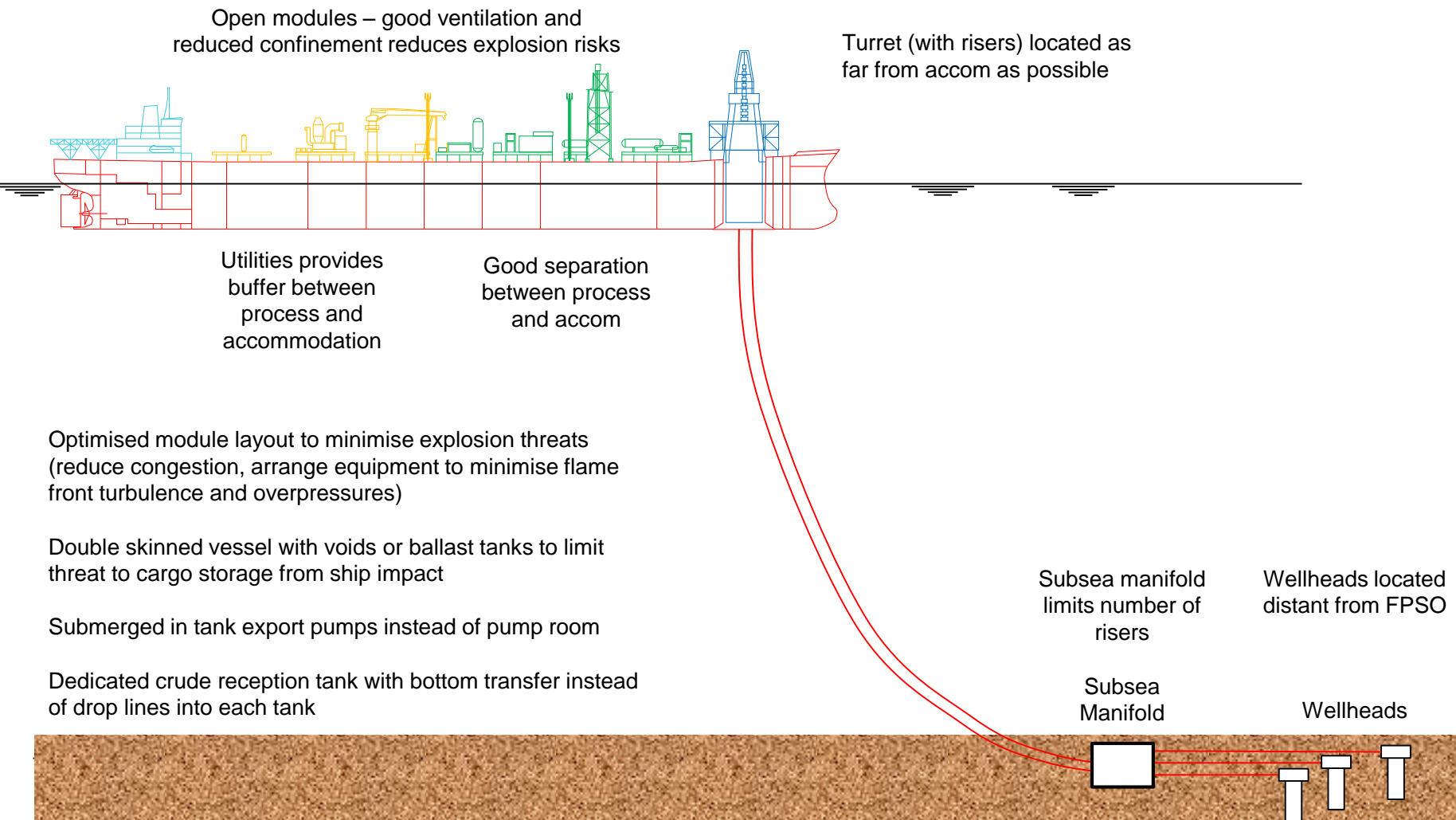
Building Safety into the Concept – Inherently Safe Design

- ☐ Minimise
- ☐ Substitute
- ☐ Segregate
- ☐ Simplify
- ☐ Intensify



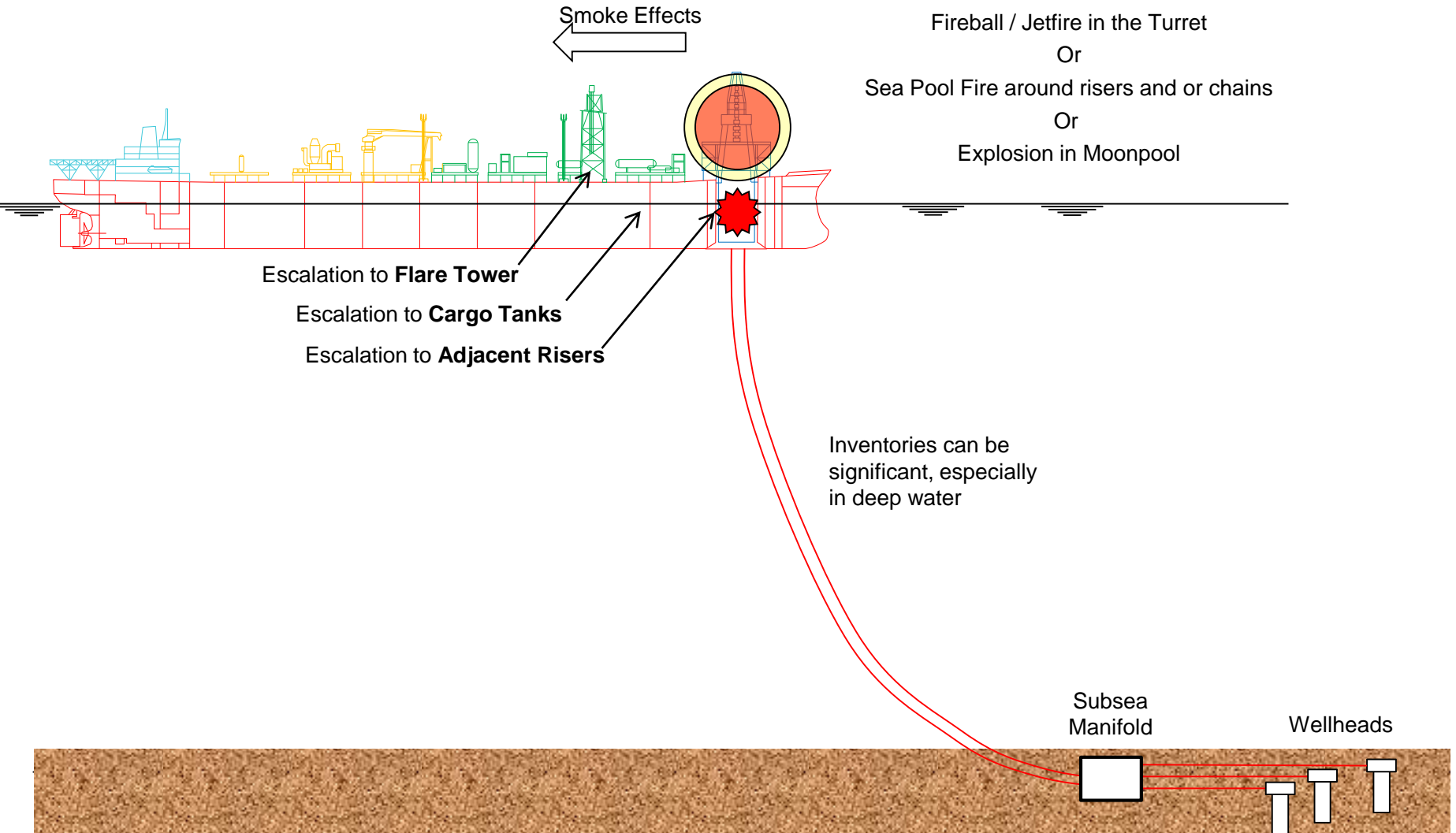
- ☐ Fewer hazards
- ☐ Fewer causes
- ☐ Reduced severity
- ☐ Fewer consequences

Building Safety into the Concept – Inherently Safe Design Features / Options



FPSO Hazards

Risers Fire / Explosion



☐ Prevention

- Process integrity, Inherently Safe Design (ISD), minimise outboard leak sources, ignition control

☐ Mitigate / Control

- Fire and gas / ESD system, pressurised TR / HVAC, intakes in safe location, TR fire/blastwall
- Also possibly riser PFP, turret deluge, emergency disconnect, subsea isolation

☐ Recovery

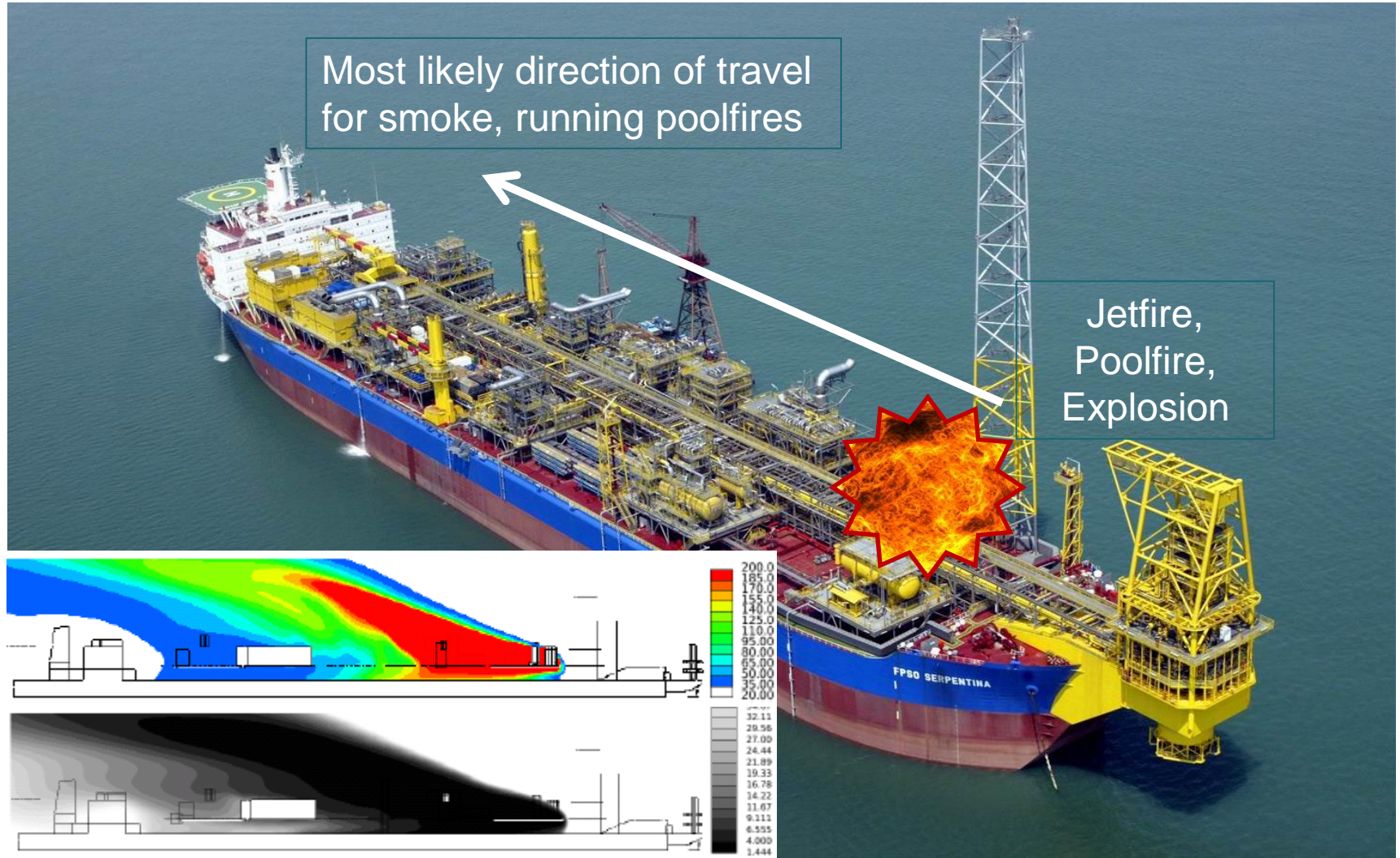
- Diverse, redundant escape routes, Protected TR, Redundant evacuation facilities

☐ FSA findings:

- Potential for personnel to be trapped on turret upper levels – restrict access and ensure multiple diverse routes area available
- If turret is close to accom then muster could be impaired – consider a pressurised tunnel in addition to evac facilities at opposite end of FPSO
- Fire/blast rating of TR bulkhead should be based on results of FEA
- Locating TR intakes in “safe” location is important – low on other side of accommodation from process
- Avoid clear line of sight between topsides leak sources and outboard sections of riser

FPSO Hazards

Topsides Fire / Explosion



☐ Prevention

- Process integrity, Inherently Safer Design, minimise dropped object threat, ignition control

☐ Mitigate / Control

- Fire and gas / ESD system, pressurised TR / HVAC, intakes in safe location, TR fire/blastwall, module deluge, main deck foam deluge and monitors, bunding & drainage
- Also possibly PFP on vessels & structures (e.g. Flare)

☐ Recovery

- Diverse, redundant escape routes, Protected TR, Redundant evacuation facilities, escape equipment

☐ FSA findings:

- Fuel gas to main power generation – potential for jetfire impacting accommodation
- Jetfire impact on cargo tank tops where there is line of sight
- Fire impact on flare, PFP may be required
- Running poolfires could impact accommodation directly, transverse coaming
- Gas build up below process modules (reduced ventilation in this area leads to potential for large gas volumes and high overpressures)
- Possible need to protect LER (fire, blast rating)
- Potential for trapping personnel on crane – protected escape routes, escape equipment
- Potential for trapping personnel on elevated platforms. Restrict access to these areas.
- Emergency systems (F&G, PA, firewater, emergency power etc) – redundancy of supply, fire resistant cabling etc

FPSO Hazards

Crude Oil Tanks – Fires & Explosions



- ☐ Largest single inventory, extensive thermal radiation, large amount of smoke
- ☐ Explosions through flammable atmosphere formation (e.g. IG failures, human error during tank prep) and ignition (static e.g. Tank washing, pyrophors)
- ☐ Escalation from other events (fire, explosion, impact)
- ☐ Environmental risk
- ☐ Intertank escalation

FSP0 Hazards

Crude Oil Tanks – Prevent , Mitigate/Control, Recover

❑ Prevention

- IG system, Process integrity, ISD, minimise dropped object threat, ignition control
- Control of tank operations e.g. Offloading, inerting, gas freeing, etc

❑ Mitigate / Control

- Very difficult to control
- Main deck foam deluge & monitors
- Pressurised TR HVAC intakes in safe location



❑ Recovery

- Most likely response to COT fire will be to evacuate
- Diverse, redundant escape routes, Protected TR, Redundant evacuation facilities, escape equipment
- Trapping of personnel for'd more likely - forward protected muster location and evacuation facilities

❑ FSA findings:

- Important to prevent escalation to COTs
- Avoid line of sight between topsides release sources and COTs
- Provision of double skinned hull to limit ship impact hazard e.g. Supply boat location
- Avoid lifting over exposed COTs or protect
- Note locations of cargo tank hatches with respect to potential main deck pool fire locations and ensure provision of fire rated seals

FSPO Hazards

Ship Collision

- ❑ Consequences of ship impact can be serious if COT ruptured
- ❑ Potential for sea pool fires and large environmental release
- ❑ Threats from:
 - Passing vessels (powered, drifting)
 - Supply boats (low energy)
 - Threat from shuttle tankers (high energy) – can impact stern directly and threaten accommodation



FPSO Hazards

Ship Collision – Prevent , Mitigate/Control, Recover

❑ Prevention

- Passing Vessel (communications, ARPA, standby vessel)
- Supply Boats (operational controls)
- Shuttle tanker (operational controls, optimise standoff distance)

❑ Mitigate / Control

- Hull structural design
- Double skinned vessel (ballast tanks, void spaces)
- Supply boat operations e.g. Protect COT via void spaces, fendering

❑ Recovery

- Passing vessels - should be some warning allowing emergency response
- Low energy supply boat collisions – should be limited consequences
- High energy shuttle tanker collisions – could cause serious damage e.g. to stern but may not cause a serious hydrocarbon release
- Emergency disconnect?

❑ FSA Findings

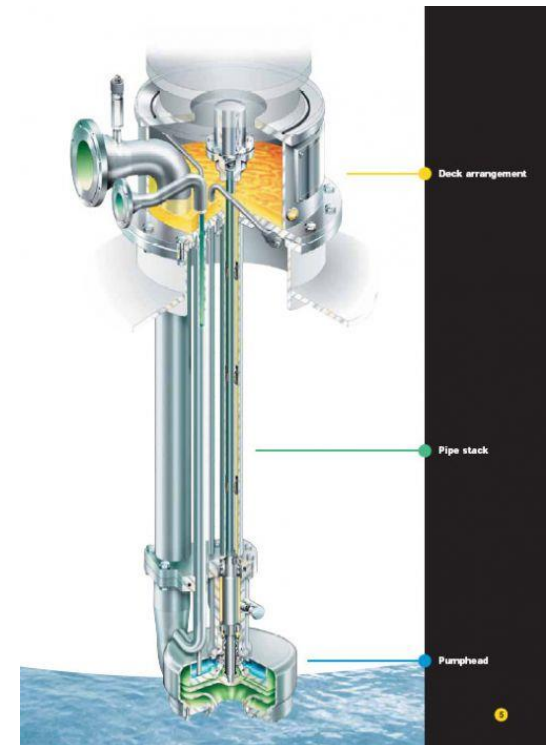
- Possible impact of exhausts / venting on supply boat ops



FPSO Hazards

Pump Room / Engine Room Fires & Explosions

- ❑ Common threat on FPSOs, trading tankers etc
- ❑ Fuel gas releases (explosion and fire), diesel or crude releases (pool fires)
- ❑ Enclosed spaces, reduced ventilation, congested / confined areas leads - explosion threat (especially pump room)
- ❑ Proximity to the accommodation and lifeboats
- ❑ Engine room / accommodation space ventilation systems can be shared – smoke migration
- ❑ Escape can be difficult, tackling fires can be difficult
- ❑ Other hazards include releases of toxic gas in confined space e.g. inert gas, nitrogen.



FSP0 Hazards

Pump Room / Engine Room – Prevent , Mitigate/Control

☐ Prevent

- Process integrity, ISD, ignition control, use of non-combustible materials
- Operational controls e.g. Housekeeping

☐ Mitigate / Control

- Fire and gas detection, ESD System, fixed extinguishing systems (e.g. inergen, CO2, high expansion foam), manual firefighting, restrict access to pump room space

☐ Recovery

- Multiple diverse escape routes from engine/pump room,
- Redundant evacuation facilities
- Muster to alternative location on main deck for example
- Emergency planning



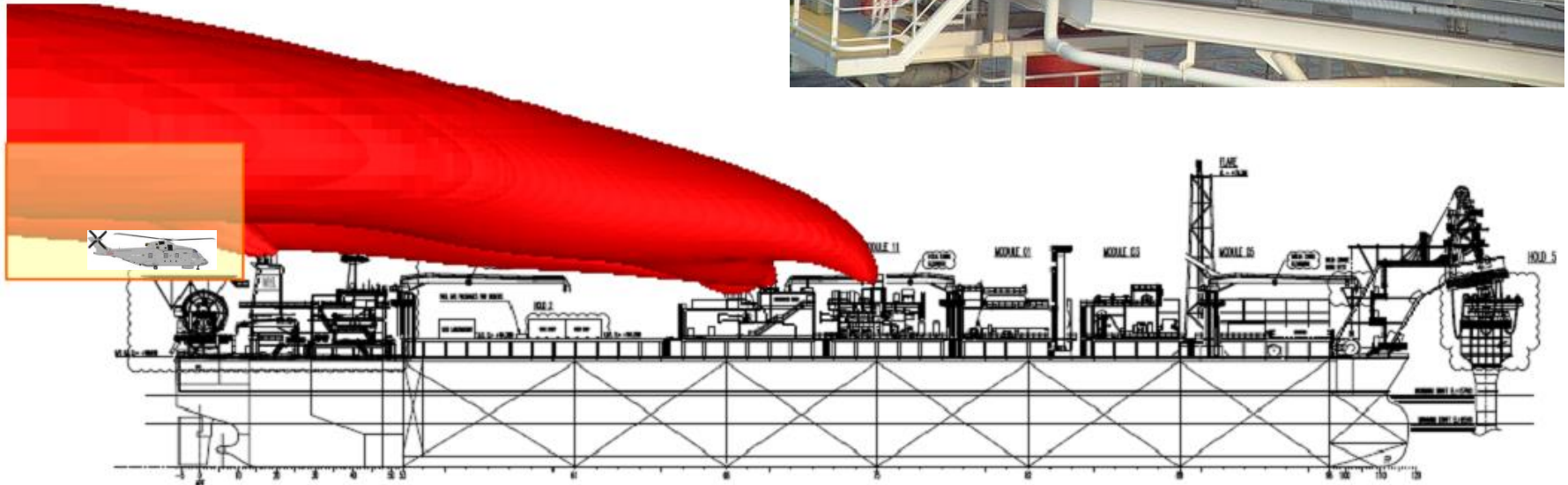
☐ FSA Findings:

- Pump room challenges – control threat by restricting access, provide escape equipment or escape trunk, provide means of removing injured parties (winch)
- Can remove pump room threat by designing space out e.g. submersible export pumps
- For'd muster locations should be protected and have comms facilities (internal & external)
- Release of extinguishment should be strictly controlled

FPSO Hazards

Helicopter Operations

- ❑ Crew changeover, shuttling operations
- ❑ Threat during flight, take off / landing
- ❑ Threat to installation – helicopter crash, refuelling facilities
- ❑ Exhausts / venting impact on heli-ops
- ❑ Structures / obstructions impact on heli approach
- ❑ Increased trips / flight duration increases risks



FSPo Hazards

Helicopter Operations – Prevent, Mitigate / Control, Recover

❑ Prevent

- Control of contractors
- Design (prevent exhaust / venting impacts, structures impact, codes & standards e.g. Navais etc)
- Refuelling facilities integrity and operations control

❑ Control / Mitigate

- Helideck fire teams, fire fighting facilities
- Refuelling - manned operation, control of ignition, firefighting response etc

❑ Recover

- Emergency response plans including rescue and recovery facilities

❑ FSA Findings

- Exhaust impacts (power generation, boilers etc) on the helideck should be considered at an early stage



FPSO Hazards

Dropped Objects

- ❑ Supply boat operations – main deck cranes, aft stores, turret cranes etc
- ❑ Dropped objects / swinging loads impacting:
 - Personnel
 - Topsides process
 - Cargo storage
 - Subsea infrastructure
- ❑ Fire / explosion threat
- ❑ Threat to critical safety equipment
 - Fire Main
 - Cables
 - Flare Pipework



FSPo Hazards

Dropped Objects – Prevent, Mitigate / Control, Recover

❑ Prevent

- Control of contractors
- Equipment certification, inspection / testing / maintenance regime
- Personnel training and operational controls
- Design of laydown areas / lifting facilities to avoid interactions

❑ Control / Mitigate

- Laydown area design & rating
- Dropped object / swinging load protection (topsides process or Safety Critical Elements, subsea, Cargo Oil Tanks)
- Operational controls e.g. minimise lift heights
- Heavy lift – additional controls

❑ Recover

- Dependant on consequences
- e.g. Loss of containment or not
- Evacuation, Escape and Rescue facilities



FSPO Hazards

Marine Hazards (Loss of Weathervaning, Loss of Stationkeeping, Loss of Stability, Structural Failure/Severe Weather)

- ❑ Loss of Weathervaning
 - Equipment failures
- ❑ Loss of Stationkeeping
 - Equipment failures, Severe weather
 - FPSO travels outwith the acceptable riser limits – riser releases;
 - Ultimately FPSO breakout
- ❑ Loss of Stability
 - Equipment failure, Human error
- ❑ Structural Failures
 - Equipment failures, Severe weather



FSP0 Hazards

Marine Hazards – Prevent, control / Mitigate, Recovery

- ❑ Main focus on prevention
 - System integrity, maintenance and testing, training and competency
 - Operational constraints e.g. severe weather constraints
- ❑ Control / Mitigation
 - Dependent upon consequences e.g. If loss of hydrocarbon containment occurs
- ❑ Recovery
 - EER facilities, Emergency response plans, Rescue and recovery facilities



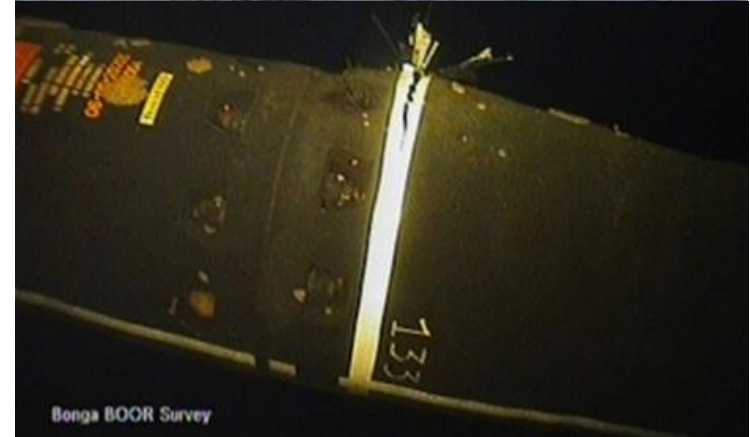
Environmental Considerations

❑ Continuous Discharges

- Combustion products from power gen (SO_x & NO_x)
- Oil/Chemicals in produced water
- Volatile Organic Compounds (VOCs) - normal operations or offloading - Particularly IG Vents
- Operational spills during maintenance

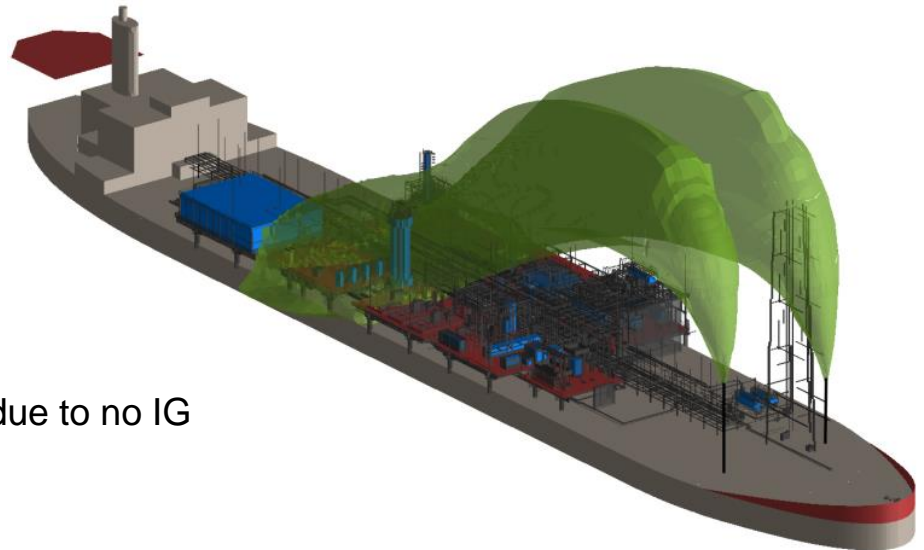
❑ Accidental Spills / Discharges

- Flaring
- Process Spills
- Riser/Pipeline breaches
- Ship Collision
- Structural Failure



Hydrocarbon Gas Blanketing & Recovery

- ☐ Hydrocarbon gas e.g. process gas used to blanket cargo tanks
- ☐ On some designs crude storage is used as a final separation stage
- ☐ Low pressure gas recovered from storage to compression train
- ☐ Most widely used particularly on NCS
 - Statoil - Asgard A (1999), Norne (2002)
 - Exxon – Jotun (2003), Balder (2004)
 - PGS Petrojarl – Varg 2006
 - Marathon – Alvheim 2008
- ☐ Pros
 - Simple System & Operation
 - Reduces need for anti-corrosive materials due to no IG
 - Reduces threat of heavy vapour slumping
- ☐ Cons
 - There may be issues due to non-availability of gas e.g. for start up or due to available volumes of gas (e.g. As fields deplete)
 - Issues can be managed by having IG back up



Inert Gas vs Blanket Gas

| Event/Hazard | Safety | | Environmental | |
|---|--------|-------------|---------------|-------------|
| | IG | Blanket Gas | IG | Blanket Gas |
| 1. Gas release from HC header. | Same | Same | Worse | Better |
| 2. Gas release from PV breaker. | Worse | Better | Same | Same |
| 3. Gas release from VRU/topsides equipment. | Same | Same | Same | Same |
| 4. Air ingress to cargo tanks. | Worse | Better | Same | Same |
| 5. Static discharge risk when loading. | Worse | Better | Same | Same |
| 6. Crude stabilisation. | Same | Same | Same | Same |
| 7. Gas blow-by to cargo tanks. | Worse | Better | Same | Same |
| 8. HC back up gas supply fails open. | Better | Worse | Same | Same |
| 9. Cargo tank overfilling. | Better | Worse | Same | Same |
| 10. Offloading rate exceeds design. | Worse | Better | Worse | Better |
| 11. Low production rate limits offloading rate. | Same | Same | Same | Same |
| 12. Prolonged process shutdown. | Better | Worse | Worse | Better |
| 13. Restart after shutdown. | Same | Same | Worse | Better |
| 14. Static discharge during COW. | Worse | Better | Same | Same |
| 15. Tank entry for maintenance. | Same | Same | Same | Same |
| 16. No blanket gas at initial start-up. | Better | Worse | Worse | Better |
| 17. No blanket gas when disconnected. | Better | Worse | Worse | Better |